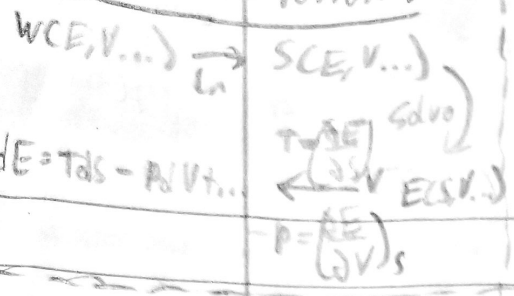
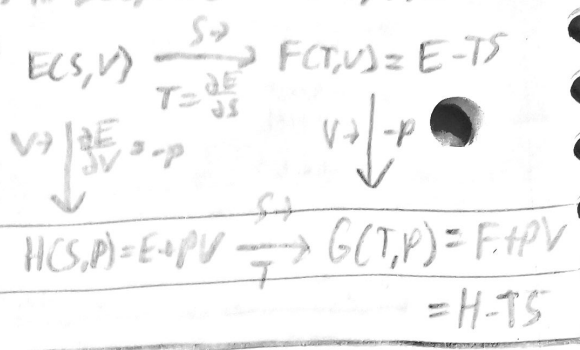
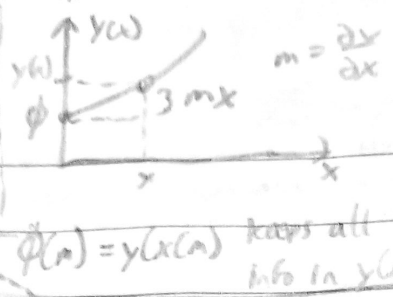


Lecture 22 review:



But what if we want variables in E(S, V...) to be T, P...?  
 can't solve E(T, P)!



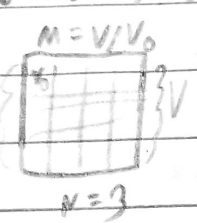
Note on derivatives:

$H = E + PV \rightarrow dH = dE + PdV + VdP$   
 $dH = TdS - PdV + PdV + VdP \rightarrow dE$   
 $dH = TdS + VdP$  (variables now S, P)  
 $T = \left(\frac{\partial H}{\partial S}\right)_P$      $V = \left(\frac{\partial H}{\partial P}\right)_S$

Lecture 23: Using Stat mech to derive useful relationships

Ex: Gas in a box (In-class exercise)

1. Specify general properties
  2. Use eqs. derived from postulates.
- (W or S, E, or H...)



$W = \frac{M!}{(M-N)!N!} \left(\frac{V}{V_0}\right)^N$

$Nk_B = n k_B = nR$   
 $S = k_B \ln W = N \ln \left(\frac{V}{V_0}\right) k_B = nR \ln \left(\frac{V}{V_0}\right)$

Heat flow & heat capacity (C)

$dV_1 = 0, dV_2 = 0$   
 $dE_1 = -dE_2$

if V and n const,  
 $dE = TdS = dq_{v,n}$

2.  $dE = TdS - PdV...$   
 $dS = \frac{1}{T}dE - \frac{P}{T}dV$

1+2:  $\frac{\partial S}{\partial V} = \frac{nR}{V} = \frac{P}{T}$   
 $PV = nRT$

$= nR \ln V - nR \ln V_0$

impossible to reach  $T=0$

E is not an explicit function of T (it is for S) but it certainly changes with T.

HWK 3.4

$dV_1 \neq 0, dV_2 = 0$   
 $dE_1 = -dE_2$

$V = \text{const}$   
 $E = \text{const}$   
 $dH = TdS + VdP$

$\left(\frac{\partial E}{\partial T}\right)_{V,n} = \left(\frac{\partial E}{\partial S}\right) \left(\frac{\partial S}{\partial T}\right) = T \left(\frac{\partial S}{\partial T}\right)_V = C_V$  (heat capacity at constant V)

$\left(\frac{\partial H}{\partial T}\right)_{P,n} = \left(\frac{\partial H}{\partial S}\right) \left(\frac{\partial S}{\partial T}\right) = T \left(\frac{\partial S}{\partial T}\right)_P = C_P$  (at constant P)

$dS = \frac{dH}{T} = \frac{dq_{p,n}}{T}$